



## Short communication

Electrochemical characterization of  $\text{La}_{0.6}\text{Ca}_{0.4}\text{Fe}_{0.8}\text{Ni}_{0.2}\text{O}_{3-\delta}$  perovskite cathode for IT-SOFC

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## HIGHLIGHTS

- $\text{La}_{0.6}\text{Ca}_{0.4}\text{Fe}_{0.8}\text{Ni}_{0.2}\text{O}_3$  electrodes were studied by impedance spectroscopy.
- The electrodes were produced at a range of different sintering temperatures.
- An equivalent circuit was constructed to describe the polarization losses.
- Cell sintered at 750 °C exhibits favorable oxygen reduction reaction properties.

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## ABSTRACT

Electrolyte supported symmetric cells featuring  $\text{La}_{0.6}\text{Ca}_{0.4}\text{Fe}_{0.8}\text{Ni}_{0.2}\text{O}_3$  (LCFN) electrodes are studied by electrochemical impedance spectroscopy. The aim is to describe the polarization losses of this mixed ionic electronic conductor electrode at various cell operating conditions for cells sintered at different temperatures. An equivalent circuit describing the cathode polarization resistances was constructed from analyzing impedance spectra recorded at different oxygen partial pressures and temperatures. Favorable oxygen reduction reaction properties are demonstrated for the LCFN cell sintered at 750 °C with a polarization resistance of 0.05  $\Omega \text{ cm}^2$  at an operating temperature of 800 °C in pure oxygen.

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## 1. Introduction

Solid oxide fuel cells (SOFC) are electrochemical devices which convert chemical energy directly into electrical energy with high efficiency and low environmental impact [1]. In order to limit cathode overpotential the traditional SOFC, with an yttria-stabilized zirconia (YSZ) electrolyte and a strontium-doped lanthanum manganite (LSM) cathode, typically operates at relatively high temperatures (800–1000 °C). These high temperatures increase balance of plant costs and encourage certain types of cell degradation [2] – making a lower operating temperature (600–

800 °C) desirable. Cells which operate in this lower temperature range are known as intermediate temperature SOFCs (IT-SOFC). In order to operate at IT-SOFC temperatures, new cathode materials are required and the processing routes must be optimized. SOFC materials development also requires further insight into the mechanisms responsible for the overpotential losses in the cathode material, for which Electrochemical Impedance Spectroscopy (EIS) is a powerful investigative tool.

In this work, electrolyte supported symmetrical cells featuring  $\text{La}_{0.6}\text{Ca}_{0.4}\text{Fe}_{0.8}\text{Ni}_{0.2}\text{O}_3$  (LCFN) electrodes were produced as previously described at a range of different sintering temperatures ( $T_s$ ) [3]. The symmetric cell configuration was chosen to study the cathode processes as the data interpretation is simpler compared to a full SOFC analysis. To determine the resistance of the various cathode processes, the manufactured cells were characterized by EIS between 600 and 800 °C and at several oxygen partial pressures ( $p\text{O}_2$ ). In addition to complex non-linear least squares (CNLS) fitting

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of the impedance spectra (IS), the distribution of relaxation time (DRT) of the IS was investigated to provide a model-independent insight into the cathode processes [4].

## 2. Experimental

### 2.1. Cell specifications

The cells used for the electrochemical testing in this study are electrolyte supported symmetric cells produced at the Technical University of Denmark (DTU). LCFN was prepared by the liquid mix method described elsewhere [5]. The cell consists of a 200  $\mu\text{m}$  thick, dense, 8 mol%  $\text{Y}_2\text{O}_3$  stabilized  $\text{ZrO}_2$  (YSZ) electrolyte produced via tape-casting, sandwiched between two LCFN electrodes, each deposited by a spray casting technique. A series of symmetric cells were produced sintered from 750 to 1000  $^\circ\text{C}$ , at increments of 50  $^\circ\text{C}$ . The shorthand notation of  $T$ -cell will be used throughout, where  $T$  represents the  $T_s$  of the symmetric cells. Details of the cathodes' structural properties and the cells' microstructure are given elsewhere [3].

### 2.2. Cell test set-up

The cell dimensions were  $5.0 \times 5.0 \text{ mm}^2$ . Pt-paste was applied onto the electrode surfaces for current collection. The test rig used for the experiments had four sample positions. At least two identical symmetrical cells were placed in the set-up and measured simultaneously in order to check reproducibility.

### 2.3. Electrochemical impedance spectroscopy

EIS was measured at open circuit voltage (OCV) with a Solartron 1260 Frequency Response Analyzer between 600 and 800  $^\circ\text{C}$ , in the frequency range  $10^6$ –0.05 Hz with 12 points/decade. IS were recorded at three different  $p\text{O}_2$  (0.2, 0.5 and 1 atm) for the 750-cell and at 1 atm for all other cells. The desired  $p\text{O}_2$  was obtained by mixing  $\text{O}_2$  and  $\text{N}_2$ . IS were analyzed using Scribner Associates' Zview software.

### 2.4. Morphological characterization – post-test analysis

Polished cross sections of the symmetrical cells after electrochemical tests were investigated by scanning electron microscopy (SEM) using a Zeiss Cross-beam 1540XB equipped with a field-emission gun.

## 3. Results and discussion

### 3.1. Qualitative analysis of impedance spectra – equivalent circuit model development

The 750-cell was chosen to develop the equivalent circuit for the LCFN/YSZ/LCFN symmetric cell. IS were recorded at different temperatures and  $p\text{O}_2$ . The data was first analyzed in terms of DRT with the peak shapes and features providing information on the nature of the contributing processes.

Fig. 1 shows DRT spectra obtained at three different  $p\text{O}_2$  for the 750-cell at 650  $^\circ\text{C}$ . In all the DRT spectra two peaks are observed – one symmetrical peak at high frequencies ( $f_{\text{peak}} \sim 10^5 \text{ Hz}$ ) and one asymmetrical peak at lower frequencies ( $f_{\text{peak}} \sim 70$ –270 Hz). The high frequency peak is weakly  $p\text{O}_2$  dependent and can be described well by a parallel RQ-element. The summit frequency for the lower frequency peak shifts to higher frequencies with increasing  $p\text{O}_2$ . The contribution of this peak is more complex but can be well described by an RQ-element and a Gerischer element in series. An

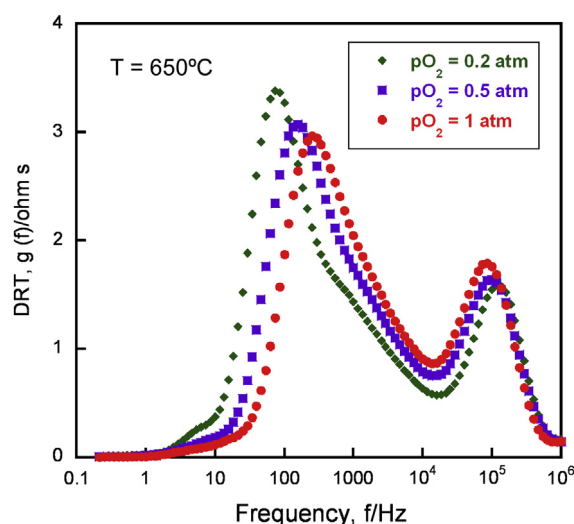


Fig. 1. DRT spectra obtained from IS obtained on the 750-cell at a  $p\text{O}_2$  of 0.2, 0.5 and 1 atm at 650  $^\circ\text{C}$ .

additional peak is observed in the  $p\text{O}_2 = 0.2 \text{ atm}$  spectra at very low frequencies ( $< 10 \text{ Hz}$ ), but is completely absent in the 1 atm spectra. This process is assigned to oxygen gas diffusion and has not been included in the equivalent circuit modeling due to its small/negligible contribution to  $R_p$ . These results are in good agreement with the kinetics of porous mixed-conducting oxygen electrodes described by Adler et al. [6]. The resulting equivalent circuit from the DRT analysis is  $L$ – $R_s$ – $RQ_1$ – $RQ_2$ – $G$ . The values, presented in the following section, are from CNLS fitting the IS with this equivalent circuit. The applied model is in good agreement with those reported in literature for similar cathode materials [7,8].

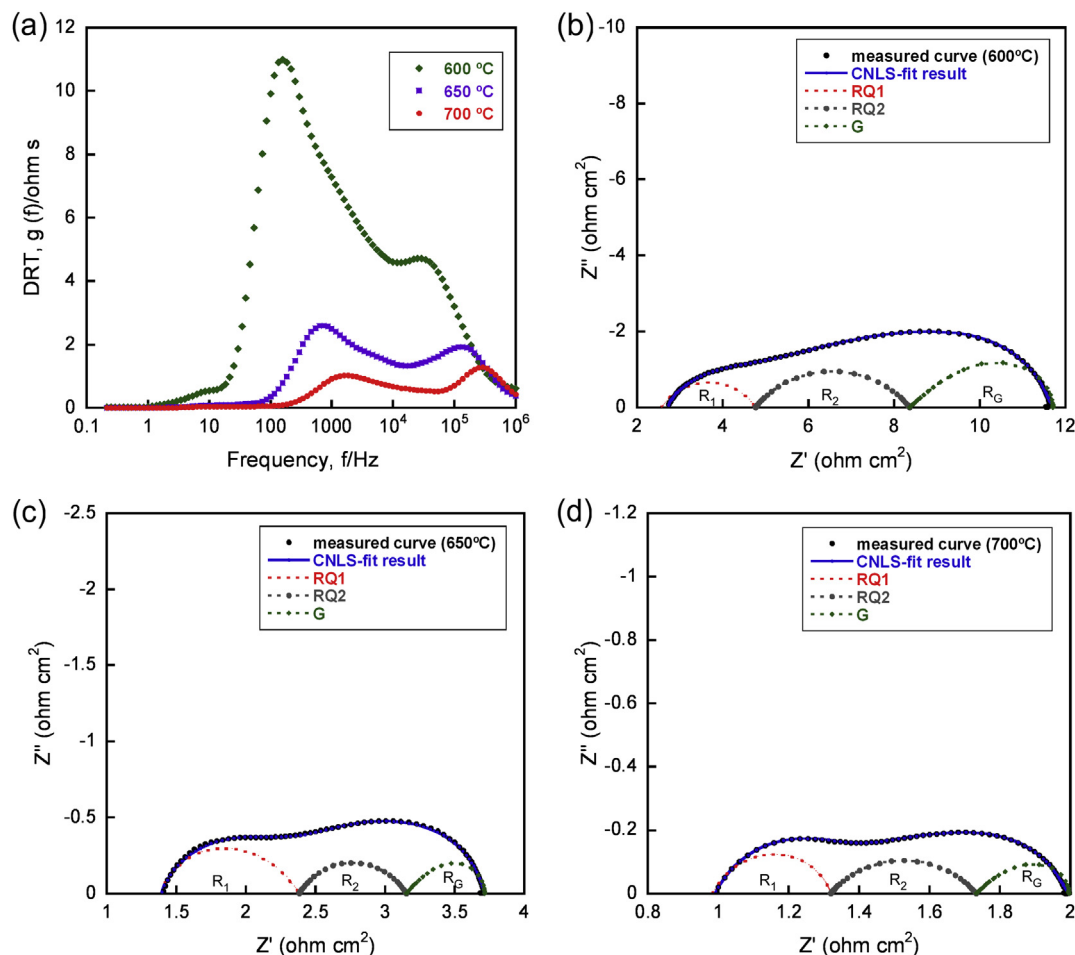
### 3.2. Quantitative analysis of impedance spectra – CNLS fitting

Fig. 2 shows the DRT and IS at  $p\text{O}_2 = 1 \text{ atm}$ , recorded at 600, 650 and 700  $^\circ\text{C}$  together with CNLS fit results. The individual  $R_p$  circuit element responses, from the  $L$ – $R_s$ – $RQ_1$ – $RQ_2$ – $G$  model, are included in Fig. 2(b–d). This shows that the  $R_p$  response described by the Gerischer element is found at the lowest frequencies. Similar fits were obtained for the other symmetrical cells.

Fig. 2a shows that the DRT peaks shift toward high frequencies with increasing temperature. Furthermore, the intermediate to low frequency range features dominate the  $R_p$ . Table 1 summarizes the main CNLS fit results and calculated activation energies for each process. The  $R_p$  value trends (Table 1) correspond well with the qualitative observations made for Fig. 2 i.e. 1) the  $R_p$  decreases with increasing temperature and 2) the intermediate and low frequency  $R_p$  contributions dominate the cells' resistance. The  $R_p$  circuit elements' activation energies are 1.15, 1.60 and 1.88 eV for the high, intermediate and low processes, respectively. Fig. 3 identifies, schematically, the location of these electrode processes according to the fitting.

The high frequency process ( $E_a = 1.15 \text{ eV}$ ;  $f_{\text{summit}} \sim 100 \text{ kHz}$  at 650  $^\circ\text{C}$ ) is independent of  $p\text{O}_2$ , and has an  $E_a$  similar to the  $E_a$  for oxide ion migration at grain boundaries in YSZ electrolyte (1 eV) [9]. This process is assigned to oxygen ion transfer from the MIEC to oxygen vacancies in the electrolyte (Fig. 3e) [13].

In contrast to the high frequency arc, the lower frequency arcs are  $p\text{O}_2$  sensitive. The arc observed at intermediate frequency ( $E_a = 1.6 \text{ eV}$ ;  $f_{\text{summit}} = 1500 \text{ Hz}$  at 650  $^\circ\text{C}$ ,  $RQ_2$ ) and low frequency ( $E_a = 1.88 \text{ eV}$ ;  $f_{\text{summit}} = 559 \text{ Hz}$  at 650  $^\circ\text{C}$ , Gerischer) are assigned to the dissociative adsorption of  $\text{O}_2$  (Fig. 3a & b) followed by



**Fig. 2.** DRT spectra at 600, 650 and 700 °C for the 750-cell at  $p_{O_2} = 1$  atm (a) and IS and corresponding CNLS fit results for IS recorded at 600 °C (b), 650 °C (c) and 700 °C (d). Dotted lines in (b), (c) and (d) represent the individual elements ( $RQ_1$ – $RQ_2$ –Gerischer) in the CNLS fit.

electrochemical reduction (Fig. 3c) and transfer of oxygen species to the electrode–electrolyte interface (Fig. 3d) [6,14]. More specifically, the intermediate frequency process is ascribed to dissociative adsorption, transfer of species at the TPB and surface diffusion [10] and the low frequency contribution reflects competitive elementary processes in the electrochemical reduction mechanism (Fig. 3c) [11]. This low frequency process had been suggested to limit the performance of both the LCFN and  $La_{0.6}Ca_{0.4}MnO_3$  cathodes based on the activation energy,  $p_{O_2}$  dependence and the characteristic frequency observed [12]. The Gerischer impedance is applied to describe MIEC electrode responses in systems where an electrochemical reaction is coupled to an oxide ion diffusion process along different pathways i.e. through the bulk, at the surface or a combination of both. This element suggests that bond breaking

and surface diffusion maybe rate limiting for the electrochemical reduction process [15].

### 3.3. Electrode microstructure after electrochemical tests

Fig. 4 shows the SEM images of cross-sections of the LCFN/YSZ/ LCFN symmetrical cells sintered at 800, 900 and 1000 °C after electrochemical testing. The 750-cell shows no discernible difference from that sintered at 800 °C. SEM analysis prior to testing is reported in our previous publication [3]. LCFN grain size and electrode density both increase with  $T_s$ . This is accompanied by a significant reduction of LCFN porosity which reduces the LCFN-surface/gas interface. Additionally,  $CaZrO_3$  formation is observed at the cathode/electrolyte interface from 850 up to 1000 °C. The  $CaZrO_3$  layer thickness increases with  $T_s$ , with only the 1000-cell exhibiting noticeable change post-electrochemical testing (increasing from 400 to 600 nm). SEM investigations therefore reveal little change in LCFN grain size, interaction layer or electrode density as a result of electrochemical testing, indicating no detrimental effects.

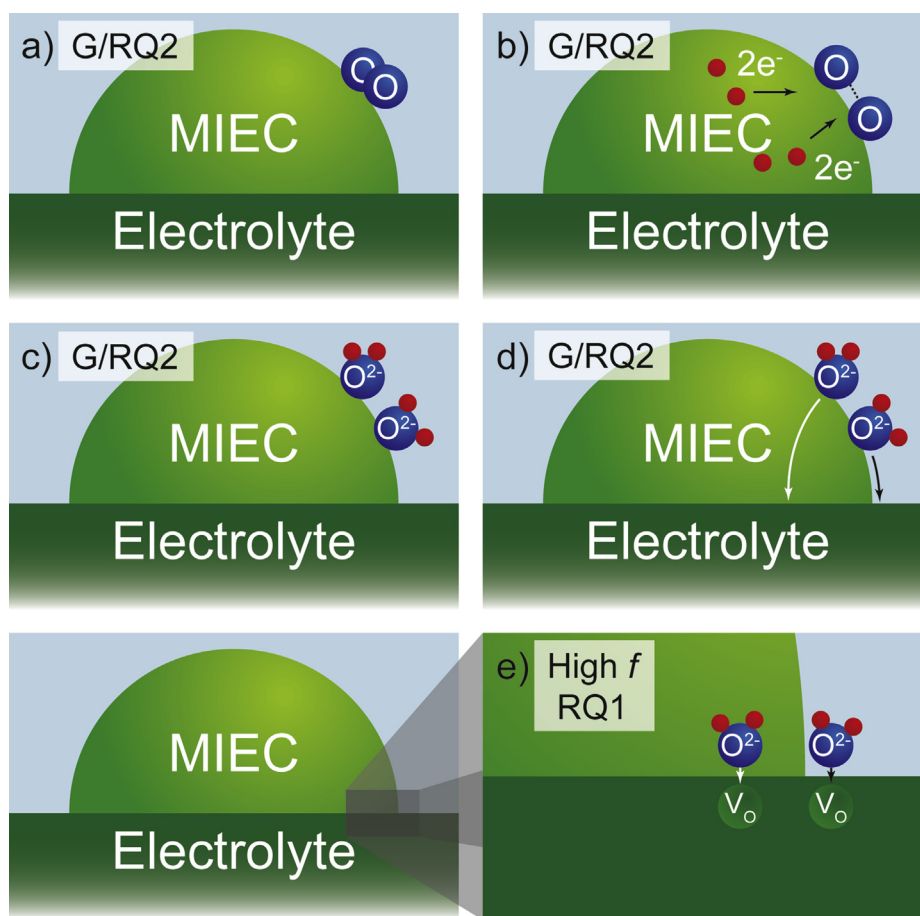
### 3.4. Effect of sintering temperature on the electrochemical performance

Table 2 summarizes the  $R_p$  and  $R_s$  for the 750-cell, 800-cell and 1000-cell. The 750-cell, first reported in the present work, has the smallest  $R_p$  of all the tested symmetrical cells with an  $R_p$  of

**Table 1**

Summary of CNLS fitting results of inductance corrected IS recorded at  $p_{O_2} = 1$  atm for the 750-cell at 600 °C, 650 °C and 700 °C. Also included are the calculated activation energies ( $E_a$ ) for each process. Resistances ( $R$ ) in  $\Omega \text{ cm}^2$ , characteristic frequencies ( $f$ ) in Hz.

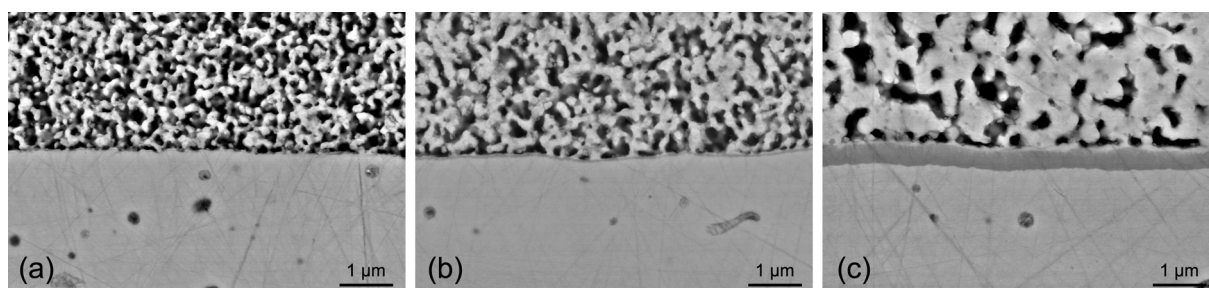
	600 °C	650 °C	700 °C	$E_a$ (eV)
$R_s$	2.57	1.20	0.87	1.27
$R_1$	2.19	1.18	0.45	1.15
$f_1$	33000	100000	300000	
$R_2$	3.606	0.77	0.41	1.60
$f_2$	760	1500	5300	
$R_G$	3.34	0.56	0.26	1.88
$f$	150	559	1510	



**Fig. 3.** Schematic of the proposed LCFN electrode processes. a)  $O_2$  adsorption, b) O dissociation; c) electrochemical reduction to  $O^{2-}$ ; d)  $O^{2-}$  migration to electrode/electrolyte interface and e) incorporation into O vacancies in YSZ electrolyte.

$0.05 \Omega \text{ cm}^2$  at  $800^\circ\text{C}$  and a  $pO_2$  of 1 atm. Increasing  $T_s$  increases  $R_p$ . The  $R_p$  of the 750-cell shows a marked improvement of 60% compared to that of the 800-cell. The  $R_p$  values are comparable with those obtained for the high-performing  $(\text{La,Sr})(\text{Fe,Co})\text{O}_3$  cathode [16]. Increasing the  $T_s$  increases the  $R_p$ , due to 1) the formation of an insulating  $\text{CaZrO}_3$  phase at the electrode/electrolyte interface and 2) the loss of electrode porosity [3]. As the  $\text{CaZrO}_3$  insulating layer is comparatively thin (ca. 400 nm for 1000-cell prior to testing) with respect to the electrolyte thickness (200  $\mu\text{m}$ ), the  $R_s$  is not significantly affected within the  $T_s$  range investigated (800–1000  $^\circ\text{C}$ ). The LCFN/YSZ/LCFN symmetric cells sintered at low temperatures (750, 800  $^\circ\text{C}$ ) show the smallest grain size and most open porosity, thus resulting in large LCFN surface area and lower  $R_p$  values.

To the best of our knowledge, this is the first time a symmetric cell for SOFC application has been sintered at such low temperature (750  $^\circ\text{C}$ ), which provides new possibilities for a more economical production route. Furthermore, a cathode  $T_s$  of only 750  $^\circ\text{C}$  is highly relevant for metal-supported SOFCs and in general for SOFCs where nano-sized particles are impregnated for increased catalytic activity [17]. The LCFN cathode performance is better than the state-of-the-art  $(\text{La,Sr})(\text{Fe,Co})\text{O}_3$  on  $\text{Y}_{0.08}\text{Zr}_{0.92}\text{O}_{1.96}/\text{Gd}_{0.1}\text{Ce}_{0.9}\text{O}_2$  electrolyte with a  $R_p$  value of  $0.142 \Omega \text{ cm}^2$  in air at 850  $^\circ\text{C}$  when sintered at 1400  $^\circ\text{C}$  [18] and better than  $\text{LaSrMnO}_3$  on YSZ electrolyte with a  $R_p$  value of  $9 \Omega \text{ cm}^2$  in air at 700  $^\circ\text{C}$  when sintered at 1250  $^\circ\text{C}$  (this work:  $0.56 \Omega \text{ cm}^2$  for the 750-cell) [19]. Similar values have been obtained for the LSM/YSZ composite at 850  $^\circ\text{C}$  with  $R_p$  values of  $0.115 \Omega \text{ cm}^2$  in oxygen [14]. The development of the equivalent



**Fig. 4.** SEM images of the cross section of LCFN/YSZ/LCFN symmetric cells after electrochemical tests: (a) 800-cell, (b) 900-cell and (c) 1000-cell.

**Table 2**

$R_s$  and  $R_p$  obtained from CNLS fitting IS on the 750-cell, 800-cell and 1000-cell at temperatures from 600 °C to 850 °C. Resistances are given in  $\Omega \text{ cm}^2$ . Measured at  $p\text{O}_2 = 1 \text{ atm}$ .

Characterization temperature (°C)	750-Cell		800-Cell		1000-Cell	
	$R_s$	$R_p$	$R_s$	$R_p$	$R_s$	$R_p$
600	2.57	4.56	4.18	4.25	3.96	2444
650	1.2	1.25	2.25	1.99	2.95	1266
700	0.87	0.56	1.32	0.72	1.68	407
750	0.57	0.16	0.85	0.23	1.07	125
800	0.41	0.05	0.61	0.08	0.58	42

circuit model increases the understanding of the nature of the processes involved and can be taken as a first indication that the oxygen surface exchange and/or partial ionic conductivity influence the LCFN electrode performance.

#### 4. Conclusions

$\text{La}_{0.6}\text{Ca}_{0.4}\text{Fe}_{0.8}\text{Ni}_{0.2}\text{O}_3$  material has been developed as an intermediate temperature solid oxide fuel cell cathode material with excellent electrochemical performance. Symmetric cells were fabricated using yttria-stabilized zirconia as the electrolyte. An equivalent circuit model was developed for analysis of impedance spectra and used for characterization of the individual polarization losses observed. This was achieved by CNLS fitting and analysis of DRT for impedance spectra from 600 to 800 °C in  $p\text{O}_2$  from 0.2 to 1 atm. To describe the processes in the cathode an equivalent circuit models described by  $L-R_s-RQ_1-RQ_2-G$  was applied. The 750-cell reveals a high electrochemical performance with an  $R_p$  of  $0.05 \Omega \text{ cm}^2$  at 800 °C.

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